

Filamentous organism bulking in nutrient removal activated sludge systems. Paper 3: Stimulation of the selector effect under anoxic conditions

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Abstract

Intermittently fed, fill and draw (IFFD) systems and continuously fed completely mixed (CFCM) systems, both having anoxic/aerobic mass fractions of 25 and 76% respectively, did not develop low F/M filament bulking sludges. Although the IFFD conditions induced a selector effect it could not be concluded that the selector effect controlled low F/M filament bulking in the system because the CFCM system, which did not induce a selector effect, also did not bulk. The selector effect induced in the IFFD system controlled *Sphaerotilus natans* proliferation, but this filament is not found in South African full-scale activated sludge plants. From anoxic batch tests a design procedure for anoxic selectors, fully integrated into current activated kinetic models, is presented. Because the low F/M Filaments prevalent in full-scale N and N & P removal plants did not develop in the laboratory-scale systems, no conclusion can be made regarding the role of selectors (anoxic or aerobic) in control of these filaments.

List of symbols

a	= mixed liquor recycle ratio from the aerobic to the primary anoxic reactor with respect to Q_{iADWF}	f_{xv}	= selector sludge mass fraction, i.e. traction of the mass of VSS in the system that is in the selector reactor(s)
a_{opt}	= a-recycle ratio that loads the primary anoxic reactor to its denitrification potential	h	= hour
ADWF	= average dry weather flow	IAWQ	= International Association for Water Quality
AVSS	= active heterotrophic organism VSS concentration (mg AVSS/l)	IFFD	= intermittently fed fill and draw
b_H	= heterotrophic organism endogenous respiration rate (/d)	K ₁	= initial rapid rate of denitrification in the primary anoxic reactor utilising RBCOD in mg NO ₃ -N/(mgAVSS-d)
	= 0.24/d at 20°C	K ₂	= second slower rate of denitrification in the anoxic reactor utilising SBCOD in mg NO ₃ -N/(mgAVSS-d)
BT	= batch test	K _{ms}	= maximum specific substrate utilisation rate [mg COD/(mg AVSS-d)]
CFCM	= continuously fed completely mixed	L _r	= peak to average COD load ratio under dry weather conditions
COD	= chemical oxygen demand	min	= minute
d	= day	M	= symbol denoting mass of compound following it, i.e. MS _i ; = mass of COD load per day = $Q_r S_{t1}$ MX _v = mass of VSS in biological reactor = $V_p X_v$
DO	= dissolved oxygen (mg O/l)	MLE	= modified Ludzack-Ettinger N removal system
D _p	= denitrification potential - concentration of nitrate that can be biologically denitrified in an anoxic reactor (mg N/l influent)	MLSS	= mixed liquor suspended solids
D _{ps}	= denitrification potential of anoxic selector (mg N/l influent)	MLVSS	= mixed liquor volatile suspended solids
DSVI	= diluted sludge volume index	mV	= millivolts
f_{aw}	= fraction of VSS mass that is active organisms	N	= nitrogen
f_{bs}	= influent RBCOD fraction with respect to the biodegradable COD	N _c	= nitrification capacity - concentration nitrate generated by nitrification (mg N/l influent)
f_{kl}	= primary anoxic sludge mass fraction	NUR	= nitrate utilisation rate as mg NO ₃ -N/(l.h) or mg NO ₃ -N/(g AVSS-h)
f_{smin}	= minimum f_{kl} to ensure that all the influent RBCOD is utilised	OUR	= oxygen utilisation rate in mg O/(l.h) or mg O/l AVSS-h
f_{cv}	= COD/VSS ratio of the sludge mass synthesised		Subscripts RBCOD and SECOD denote the OUR for RBCOD and SBCOD utilisation respectively. Subscript Het is the heterotrophic OUR Which is the sum of OUR _{RBCOD} and OUR _{SBCOD}
F/M	= food to micro-organism ratio	p	= phosphorus
f_{bs}	= fraction of the total influent COD (S _{ti}) that is readily biodegradable (S _{bsi})	PDWF	= peak dry weather flow
		Q _i	= influent flow (L/d)
		Q _u	= underflow rate (lid)
		RBCOD	= readily biodegradable COD

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